



## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

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<b>(21) International Application Number:</b> PCT/GB92/00618 <b>(22) International Filing Date:</b> 7 April 1992 (07.04.92)  <b>(30) Priority data:</b> 9107378.3 8 April 1991 (08.04.91) GB  <b>(71) Applicant (for all designated States except US):</b> IMPERIAL CHEMICAL INDUSTRIES PLC [GB/GB]; Imperial Chemical House, Millbank, London SW1P 3JF (GB).  <b>(72) Inventors; and</b> <b>(75) Inventors/Applicants (for US only) :</b> JONES, Peter, John, Vaughan [GB/GB]; 25 Manor Court, Wolviston, Bil- lingham, Cleveland TS22 5LS (GB). SEGAL, John, An- thony [GB/GB]; 2 Coppice, Hawley Lane, Halebarns, Cheshire WA15 0XX (GB). WHYMAN, Robin [GB/ GB]; 25 Rowan Park, Christleton, Chester, Cheshire AH3 7AZ (GB).	<b>(74) Agents:</b> ROBERTS, Jonathan, Winstanley et al.; ICI Group Patents Services Dept., P.O. Box 6, Shire Park, Welwyn Garden City, Hertfordshire AL7 1HD (GB).  <b>(81) Designated States:</b> AT (European patent), BE (European patent), CH (European patent), DE (European patent), DK (European patent), ES (European patent), FR (Eu- ropean patent), GB (European patent), GR (European patent), IT (European patent), JP, LU (European pa- tent), MC (European patent), NL (European patent), SE (European patent), US.  <b>Published</b> <i>With international search report.</i> <i>Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>	
<b>(54) Title:</b> OLEFIN POLYMERISATION  <b>(57) Abstract</b>  Olefin polymerisation uses catalysts based on <u>pi-arene complexes of lanthanide metals</u> in particular such catalysts support- ed on <u>hydrophilic or hydroxylic surfaces particularly of alumina or silica or halide surfaces</u> particularly magnesium chloride. Such catalysts will polymerise ethylene and also propylene to give a largely isotactic polymer without using an electron donor to enhance stereo regularity. They also do not require co-catalysts to activate polymerisation.		

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### Olefin Polymerisation

This invention relates to the polymerisation of olefins, in particular 1-olefins such as ethylene and/or propylene, using as catalysts pi-arene complexes of lanthanide metals and to supported pi-arene complexes of lanthanide metals which are especially suitable as catalysts in such polymerisations.

Pi-complexes of aromatic compounds (arenes) and lanthanide metals in which the atoms of the lanthanides are in the zero valence state are known, for example, from published European Patent Specification No 0295829 A which describes a range of such compounds and their use in chemical vapour deposition techniques.

The present invention is based on our discovery that pi-arene complexes of lanthanide metals carried on supports, particularly inorganic oxide or halide supports, are active as olefin polymerisation catalysts.

Accordingly, the present invention provides an olefin polymerisation catalyst comprising a pi-arene complex of one or more lanthanide metals carried on or reacted onto the surface of a solid support.

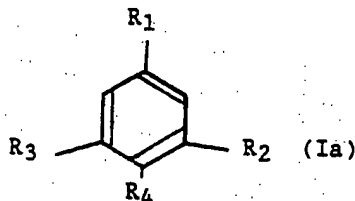
The invention includes a method of polymerising at least one olefin monomer which comprises bringing the olefin monomer(s) into contact with a catalytic amount of an olefin polymerisation catalyst comprising a pi-arene complex of one or more lanthanide metals carried on or reacted onto the surface of a solid support, thereby bringing about polymerisation of the olefin monomer(s).

The invention further includes the use of an olefin polymerisation catalyst comprising a pi-arene complex of one or more lanthanide metals carried on or reacted onto the surface of a solid support, as a catalyst in the polymerisation or copolymerisation of olefins.

The pi-arene complexes of lanthanide metals used in this invention are materials in which occupied pi-orbitals (bonding or antibonding) of an arene molecule interact with the available outer orbitals of a lanthanide metal atom. Most usually the arene is a carbocyclic, typically a benzenoid, arene compound.

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Particularly useful arenes include hydrocarbyl substituted benzenes in which there can be one or more, for example two or three, such hydrocarbyl substituents. Suitable benzenoid arena compounds can be selected from those of the formulae (Ia):



where  $R_1$  is a hydrocarbyl group;

$R_2$  and  $R_3$  are each independently a hydrogen atom or a hydrocarbyl group;

and

$R_4$  is a hydrogen atom or, when  $R_2$  and  $R_3$  are both hydrogen atoms, a

hydrocarbyl group.

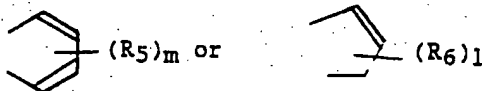
Thus arenes of the formula (Ia) include monohydrocarbyl substituted, 1,3- and 1,4-di-hydrocarbyl substituted and 1,3,5-trihydrocarbyl substituted benzenes. Further suitable arenes include compounds selected from those of the formula (Ib):



where each  $R_5$  is a hydrocarbyl group;

$n$  is 0, 1 or 2; and

A is a group of one of the formulae:



where  $R_6$  is a hydrocarbyl group;

$m$  is 0, 1 or 2; and

$l$  is 0 or 1.

30

In particular, arenes of the formula (Ib) include naphthalene and hydrocarbyl substituted naphthalenes.

Hydrocarbyl substituents in the arenes of the pi-complexes, used in this invention are particularly alkyl groups typically C<sub>1</sub> to C<sub>10</sub>, more usually C<sub>1</sub> to C<sub>6</sub>, alkyl groups e.g. methyl, ethyl, propyl, iso-propyl, butyl, iso-butyl and tert-butyl groups. Particularly suitable arenes include toluene and 1,3,5-tri-tert-butyl benzene (TTBB).

Most usually, the pi-complex will be a 2:1 (molecular) arene:lanthanide complex. We believe that such complexes exist primarily as arene:lanthanide:arene "sandwich" compounds. In such 2:1 pi-complexes the lanthanide metal atom is (formally) in the zeroth valence state. It is certain such complexes that form the subject matter of EP 0295829 A referred to above. Accordingly, the 2:1 complexes will typically have the formula (II):



where each An is independently a molecule of an arene, particularly one of

the formula (Ia) or (Ib) set out above; and  
Ld is an atom of a lanthanide metal.

The lanthanide metal used in the complex can be any lanthanide metal from lanthanum (La, Atomic No 57) to Lutetium (Lu, Atomic No 71) in the Periodic Table. Particularly suitable complexes include those of Neodymium (Nd, Atomic No 60), Samarium (Sm, Atomic No 62), Gadolinium (Gd, Atomic No 64), Erbium (Er, Atomic No 68) and Ytterbium (Yb, Atomic No 70). To date we have obtained especially good results using complexes of Gd and Er, in particular with toluene and TTBB.

The pi-arene complexes of lanthanide metals can be synthesised by methods generally known in the art. Conveniently they can be made by metal vapour synthesis as generally described in J. Chem. Soc. (Dalton), 1981, 1938 as referred to in EP 0295829 A, the disclosures of both these documents being incorporated herein by reference. The pi-complexes are typically highly coloured compounds having strong absorptions in the UV-visible region of

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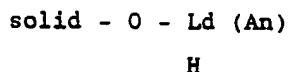
the spectrum. They are also very reactive and need suitably careful handling, keeping them well separated from reactive materials that might destroy them e.g. water or air. It may be of benefit to keep them relatively cold to reduce the likelihood of undesired reactions.

According to the invention, particularly good olefin polymerisation catalysts can be obtained by supporting the catalytic  $\pi$ -arene lanthanide complexes on a solid support material. The support material will usually be particulate and often, but not necessarily porous or spongiform to provide a large surface area for absorption or adsorption of the catalyst  $\pi$ -complex and thus a large number of available catalytic sites. The support used in the supported catalysts of this invention can be entirely inert to the catalytic properties of the complex and polymeric materials such as polypropylene, polystyrene and PEEK (polyetheretherketone). However, we have obtained particularly good results by using inorganic halides and oxides as supports. Among halides, alkaline earth metal halides are useful, especially magnesium chloride which itself may be provided as fine crystallites deposited on a base support e.g. of silica or alumina.

Among oxides those having hydrophilic and in particular hydroxylic surfaces are especially useful. Examples of such supports include silica, silicate and aluminosilicate minerals including clays, and magnesium, aluminium, zirconium and titanium oxides. Substantially pure silica and unhydrated aluminium oxide (alumina) are especially useful and the use of these materials as catalyst supports forms a specific and particularly beneficial aspect of the invention.

The  $\pi$ -arene complexes used in making supported catalysts of the invention are reactive towards inorganic halide and oxide surfaces and, thus, the practical supported catalysts will not have "sandwich" compounds of the type described above as such on their surface. The exposed surfaces of oxides, including silicates and aluminosilicates, typically have hydroxyl groups on them. This is a result of the high reactivity of the exposed hydrogen atoms which pick up hydrogen from any available water, or

other similar material, to form surface hydroxyl groups. We do not definitely know what reaction (or reactions) occur(s) between the pi-complex and the surface of the support but where the surface has, for example, surface hydroxylation we think it likely that the lanthanide metal will react with the O-H group to form a group:



This is a net insertion reaction with (starting with a 2:1 arene: lanthanide complex) loss of one molecule of arene. The pi-complexes are so reactive that we believe that they will readily undergo further reactions with closely adjacent hydroxyl groups on the surface of the support to form species which are inactive or much less active as olefin polymerisation catalysts. Thus, to maximise the number of active catalyst sites it is desirable to restrict the total number of hydroxyl groups on the surface of the support. This can be done by heating the support to reduce surface hydroxylation by driving off water or using suitable chemicals to react with and, thus, effectively remove a proportion of the surface hydroxylation. Oxide supports, as commercially available materials, such as silica and alumina can contain bound water as 'water of crystallisation' (whether or not the oxides are themselves arystalline or amorphous) as well as having surface hydroxylation. Heating silica or alumina e.g. under vacuum, to temperatures above about 300°C e.g. 350 to 500°C, for some hours e.g. 2 to 10 hours, seems to remove 'water of crystallisation' and some surface hydroxylation and significantly improves the properties of the catalyst of the invention made using the support. Event higher temperatures e.g. up to 800°C or up to 1000°C, may be beneficial in reducing hyxroxylation further. Of course, complete removal of hydroxylation would not be beneficial because it would remove binding sites for the lanthanide complex where the support is alumina, it will usually be desirable to avoid heating it to a temperature high enough to

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cause a phase change e.g. as can take place from gamma-alumina to alpha-alumina at temperatures above about 800°C.

On halide supports such as  $\text{MgCl}_2$ , we believe that the pi-complexes react with the surface but we are not sure whether the reaction is with hydroxyl species on the surface of the halide or with the halide itself. Suitable halide supports can be made by methods analogous to those used to prepare similar supports from Ziegler-Natta catalysts based on Ti(IV) species but, of course, avoiding the use of Ti e.g. as  $\text{TiCl}_4$ . Thus, to generate  $\text{MgCl}_2$  supported on silica the support making generally described in EP 0371664 A can be used but halogenating the Mg species using dry pure HCl rather than  $\text{TiCl}_4$ . Thus, the silica can be treated with a magnesium alkyl e.g. Mg butyl and then with a suitable carboxylic acid followed by treatment with HCl.

That a significant reaction is occurring between the surfaces of these supports and the pi-complexes is plain as there is a significant colour change. The typically red, blue, green or purple colour of the complex (in solution) becomes typically a dark brown colour on oxide supports (silica or alumina) and a purple colour on magnesium chloride supports. Further the colour of the solution is rapidly removed by reaction of the pi-complex with the surface.

The dimensions of the supported catalyst are primarily determined by the support. Generally particles of catalyst support will be in the range 20 to 100  $\mu\text{m}$  although where polymers are being used as supports the particles may be somewhat larger e.g. up to about 1 mm. Especially where the support is silica or alumina, or these materials are used as a base support e.g. for  $\text{MgCl}_2$ , the support will typically be porous with a specific surface area of from 10 to 2000 more usually 200 to 1000  $\text{m}^2 \text{g}^{-1}$ .

The supported catalysts can be made straightforwardly by dispersing the dry support in a solution of the pi-complex in a suitable volatile solvent removing excess liquid and evaporating off the solvent from the treated support. The supported catalysts are not as reactive as the pi-complexes themselves but are sensitive to moisture etc and suitable handling techniques will be used as are known in the art.



The processes and catalysts of the invention can be used to polymerise or copolymerise olefins. Usually the, or at least one of the, olefin monomer(s) is a 1-olefin typically a low molecular weight 1-olefin such as ethylene and/or propylene. The  
5 polymerisation can be a homopolymerisation to give, for example, polyethylene or polypropylene or a copolymerisation to give, for example, an ethylene/ propylene copolymer, or a copolymer of ethylene and/or propylene with a higher olefin e.g. 1-heptene, or a diene such as butadiene to give an EPDM type ternary copolymer.  
10 Polymerisation reactions catalysed with pi-arene complexes of lanthanide metals according to the invention do not require the presence of the co-catalysts or activators such as aluminium alkyls or halo-alkyls, as are typically needed with conventional transition metal catalysts such as those based on vanadium,  
15 chromium and titanium, rather the polymerisation reaction seems to occur freely in the presence of the pi-complex and the olefin monomer. However, the presence of such co-catalysts or activators can be tolerated by the catalysts of this invention although usually incurring some loss of activity.

20 The polymerisation can be carried out in the presence of an organic solvent or diluent (so-called 'diluent' processes), with the olefin monomer in the liquid phase providing the reaction medium (so-called 'bulk' processes) or with the olefin monomer, at least partly, in the gas phase (so-called 'gas phase' processes)  
25 in which the reactor bed of growing particles of polymer is either fluidised by the gaseous monomer or is stirred to ensure good contact between the monomer and catalyst.

The reaction conditions for successful catalytic olefin polymerisation in this invention do not need to be extreme. We  
30 have successfully carried out polymerisation at ambient temperature and pressure. Particularly at ambient pressure the effective concentration of olefin monomer(s) such as ethylene (where this is being polymerised) is low and the use of super ambient pressure can be used to speed up polymer production. In  
35 practical industrial olefin polymerisation processes the pressures used are such as to bring the reaction temperatures close to, or even below in the case of 'bulk' processes, the dew point of the

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olefin monomer. Again to increase polymer production elevated temperatures up to about 100°C, more usually up to about 80°C are commonly used. At 80°C reaction pressures of the order of about 32 bar will typically be used. Such conventional temperatures and pressures can be used in the present invention.

The polymers produced by the method of this invention typically have high molecular weights comparable with those of currently available polyolefin polymers. A difference from such typical polymers is that the products of this invention tend to have a much wider range of molecular weights (as measured by gel permeation chromatographic polydispersity) than is typical with current catalysts. This can be advantageous in deliberately broadening the molecular weight range of polyolefins, especially polypropylene, e.g. by using combination catalysts.

The catalysts of the invention are reactive towards hydrogen such that hydrogen can be used as a chain transfer agent to modify the average molecular weight of the polymer product in olefin, particularly propylene, polymerisation reactions.

The polymerisation of propylene according to the invention gives a substantially isotactic polymer without the electron donors that are needed to produce isotactic material using currently available Ziegler-Natta catalysts such as those based on Ti(IV) species. The polymerisation of propylene using the catalysts of the invention forms a specific aspect of the invention.

The invention is illustrated by the following Examples. All parts and percentages are by weight unless otherwise stated.

### Materials

#### pentane

5 was purified to remove olefins using sulphuric acid, thoroughly washed with water to remove acid residues and dried firstly over calcium chloride and then by distillation over Na/K alloy and stored in a Schenk vessek over a potassium mirror under nitrogen.

#### 10 n-heptane

was purified and stored as described for pentane.

#### alumina

15 used as support was dried in a quartz tube under vacuum ( $10^{-3}$  mbar) at 550°C for 4 hours. The vacuum was maintained during cooling and the material stored until use in the evacuated tube. Two grades of commercially available material were used Degussa grade C and Ketchen grade L.

#### magnesium chloride

20 used as support was prepared by ball milling under dry nitrogen at ambient temperature for two hours and the product stored until used under nitrogen.

#### ethylene and propylene

25 were polymerisation grade materials dried before use by passing through a drying column of 4A molecular sieves. Propylene was further purified immediately before use by passing through a trap containing potassium on glass wool.

#### metal pi-complexes

the pi-complexes used in the Examples were made by metal vapour synthesis using the technique generally described in J

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Chem.Soc. (Dalton), 1981, 1938 as illustrated by the synthesis of neodymium di(TTBB) as follows:

In a rotary metal vapour synthesis apparatus (from Torrovap Industries Inc., Ontario, Canada) metallic neodymium was evaporated using electron beam heating. This vapour was co-condensed with TTBB vapour at  $-196^{\circ}\text{C}$ . After warming to room temperature under dry argon, the product was dissolved in dry *n*-heptane removed from the reactor using an internal transfer tube and collected in a Schlenk tube as a deep burgundy red coloured solution. The solution was filtered through cellite to remove solid impurities. The solution had a measured maximum absorption at 535 nm. This is consistent for the formation of the 2:1 TTBB:neodymium pi-complex.

Further pi-complexes as set out below were also made by this method but substituting the appropriate starting materials. The pi-complexes, their colours and absorption maxima are as follows

20	pi-complex	colour	UV-vis. abs. max (nm)
	Nd di(TTBB)	deep burgundy	535
	Nd ditoluene	dark brown	
	Sm di(TTBB)	deep green	
	Gd ditoluene	blue-black	
25	Gd di(TTBB)	deep purple	548
	Er di(TTBB)	red	500

Example S1

Preparation of supported catalyst

Neodymium di(TTB) supported on silica (catalyst S1) was made by adding a solution of about 0.8 mmole of the Nd di(TTB) pi-complex, made as described above, under dry argon to a slurry of 5 g of silica (previously dried overnight at 350°C.) in dry n-heptane. The colour of the solution was discharged virtually instantaneously and the silica assumed a uniform dark brown colour. Samples of 1 g of this product were used slurried in n-heptane in performing polymerisations.

Examples S2 to S10

Using the same general method as described in Example S1, the following supported catalysts were made but substituting the corresponding pi-complex and/or support for the materials used in Example S1.

Supported on silica

S2	samarium	di(TTB)
S3	gadolinium	ditoluene
S4	gadolinium	di(TTB)
S5	erbium	di(TTB)

Supported on alumina

S6	neodymium	di(TTB)
S7	gadolinium	di(TTB)
S8	erbium	di(TTB)

Supported on magnesium chloride

S9	gadolinium	di(TTB)
S10	erbium	di(TTB)

The alumina supports were of gamma-alumina obtained from Degussa which had been dried at 500°C for at least 3 hours. Magnesium chloride supports were made by ball milling anhydrous

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catalyst grade material for 2 hours and the resulting powder was used as the support.

In addition to the supported catalysts four pi-complexes were prepared for use as unsupported catalysts for comparison under the codes U1 to U4:

U1	samarium	di(TTBB)
U2	gadolinium	ditoluene
U3	gadolinium	di(TTBB)
U4	erbium	di(TTBB)

#### Examples P1 to P17

Ethylene polymerisation reactions were carried out using the catalysts U1 to U4 and S1 to S10. The following general route was used.

A volume of catalyst slurry containing 1 g of supported catalyst was transferred via syringe to a clean dry 250 ml glass vessel containing 100 ml dry deoxygenated n-heptane or toluene (distilled over sodium wire) and through which was passed a continuous flow of dry ethylene at atmospheric pressure. The suspension was agitated and allowed to react for 1 hour at ambient temperature. The suspension gradually thickened and decolourised as polymer growth occurred. The contents of the vessel were filtered, washed with toluene and then heptane and thoroughly dried prior to weighing for yield. The polymer collected was identified as polyethylene by infra-red spectroscopy. The catalyst activity calculated from the polymer yield and the lanthanide analysis as g (polymers) mmol<sup>-1</sup> (lanthanide metal) hour<sup>-1</sup> is the average activity during the reaction. The results are set out in Table 1 below.

#### Examples P18

Propylene polymerisation reactions were carried out using the catalyst S8. The following general route was used.

An existing 4 litre capacity stainless steel autoclave equipped with an outer steam/water heating/cooling jacket and an anchor stirrer was washed with a solution of triethyl aluminium in an inert hydrocarbon diluent (alkane fraction nominal boiling at 180°C) overnight at 65°C to remove inhibitors. The traces of aluminium compound were removed by washing with diluent and the gas space then purged at 65°C by admitting 300mls of polymerisation grade liquid propylene and venting down slowly to atmospheric pressure. The catalyst component, about 5 g, as a slurry in heptane was then injected using a syringe through a serum cap on the top cover entry valve to the autoclave. 1.5 litres of liquid propylene were immediately added to the autoclave and the temperature was maintained at 65°C with stirring. Unreacted propylene was removed by evaporation and the autoclave discharged after nitrogen purging. The slurry collected was filtered, washed with heptane and dried.

Infra-red diffuse reflectance spectroscopy detected an organic component which was identified as predominantly isotactic polypropylene.

Examples P19 to P21

Further runs were carried out using various supported catalysts S7 - reaction time of 1 hour.

Infra-red diffuse reflectance spectroscopy detected an organic component which was identified as predominantly isotactic polypropylene. Raman spectroscopy using a 514nm argon laser line showed bands at 1459, 1436, 1329, 1358 and 398 wave numbers indicating the presence of isotactic polypropylene.

S9 - reaction time 1 hour (using 4 g supported catalyst containing 40mg of gadolinium suspended in 200ml n-heptane.

The product collected from this experiment was suspended in 300ml of 4M aqueous sulphuric acid and stirred at ambient temperature for 4 hours. On settling the acid layer was removed and replaced with water. After stirring the resulting slurry

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thoroughly to remove residual acid the suspension was filtered and the solid polymer recovered.

A sample of the product was pressed into a disc for analysis by infra-red spectroscopy. The product was identified as predominantly isotactic polypropylene. A small quantity of the product was dissolved in methylnaphthalene and subjected to gel permeation chromatography. This material gave an average molecular weight of 700000 D and had a polydispersity of 18.2.

S8 - reaction time 2.5 hours

Infra-red diffuse reflectance spectroscopy detected an organic component which was identified as predominantly isotactic polypropylene.

A small quantity of the product was dissolved in methylnaphthalene and subjected to gel permeation chromatography. This material gave an average molecular weight of 200,000 D and had a polydispersity of 11.1.

#### Examples S11 to S17

#### Preparation of supported catalyst

These preparations were carried out in a nitrogen filled glove box fitted with a recirculating drying and deoxygenating train.

A sample (ca. 25 mg) of a metal bisTTBB complex was placed in a 500 ml thick walled glass tubular reactor, pentane (100 ml) was added and the mixture stirred magnetically to form a solution. A portion (ca. 250 mg) of support was weighed in the glove box and added to the stirred solution in the reactor. Further pentane (ca. 30 ml) was used to wash any residual solid on the walls of the reactor into the solution.

#### Examples P22 to P28

The reactor containing the supported metal complex was used to polymerise propylene as follows. The reactor lid (having a



pressure gauge, temperature probe and a closed inlet valve) was fitted onto the top of the reactor tube and the sealed assembly was removed from the glove box and connected to the reactor manifold. Air in the system in the region of this connection was removed using a vacuum line and the reactor was pressurised to polymerisation pressure using propylene.

The suspension in the reactor vessel was stirred for a period of one hour at reaction temperature with the reactor pressure automatically maintained by a control valve between the reactor and the reservoir. No temperature control was applied during reaction. At the end of the reaction period the reactor was disconnected from the manifold and vented in a fume cupboard. The polymer product was recovered by filtration or evaporation to dryness and then drying under vacuum 10 mbar at 60°C for ca. 2 hours.

The nature of the metal complex and the support used in Examples S11 to S17 and the reaction conditions used in Examples P22 to P28 are summarised in Table 2a below and the catalyst activities assessed from the yield of polymer and properties of the polymer produced are set out in Table 2b below.

The spectra of the polymers obtained in Examples P22 to P28 by recorded using a Raman laser microscope (488 nm) indicated that all the polymers were substantially isotactic.

The polymer obtained in Example P25 was further investigated. Integration of the isotactic methyl peak (mmmm) in the  $^{13}\text{C}$  NMR spectrum (FX 270 MHz spectrometer on a solution in *o*-dichlorobenzene) as compared with all other methyls suggested that the polymer was 40.3% isotactic and the spectrum showed no sign of head to head polymerisation of propylene units.

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Table 1

Ex No	Catalyst	Medium	Activity (g.mmol <sup>-1</sup> .hr <sup>-1</sup> )
P1	S1	heptane	5.07
P2	S6	heptane	9.52
P3	U1	heptane	2.24
P4	S2	heptane	2.94
P5	U2	toluene	2.60
P6	S3	toluene	11.59
P7	U3	toluene	3.56
P8	S4	toluene	1.97
P9	S7	toluene	0.79
P10	U3	heptane	8.13
P11	S4	heptane	17.02
P12	S7	heptane	57.83
P13	S9	heptane	29.26
P14	U4	heptane	6.49
P15	S5	heptane	26.21
P16	S8	heptane	94.38
P17	S10	heptane	38.71

Table 2a

Ex No	Metal	Support	Loading (Z)	Reaction Conditions	
				Pressure (bar)	Temp. (°C)
S11	Er	Alumina	2.6	5.0	24
S12	Er	Alumina	9.4	5.0	65
S13	Er	Alumina	8	5.0	24
S14	Er	Alumina	10	8.5	24
S15	Er	Mg chloride	10	8.5	24
S16	Gd	Alumina	4.7	5.0	24
S17	Gd	Alumina	2.3	5.0	24

Table 2b

Ex No	Supported Metal Complex	Activity (g.mmol <sup>-1</sup> )	Isotactic (Z)	Head to Head (Z)
P22	S11	2.0		
P23	S12	1.0		
P24	S13	0.3		
P25	S14	1.0	40.3	0
P26	S15	4.6		
P27	S16	0.2		
P28	S17	0.2		

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## Claims

- 1 An olefin polymerisation catalyst comprising a pi-arene complex of one or more lanthanide metals carried on or reacted onto the surface of a solid support.
- 2 A catalyst as claimed in claim 1 wherein the arene is a benzenoid arene.
- 3 A catalyst as claimed in claim 2 wherein the arene is a hyrdocarbyl, particularly an alkyl, substituted benzene.
- 4 A catalyst as claimed in claim 3 wherein the arene is 1,3,5-tri-tert.butyl benzene.
- 5 A catalyst as claimed in any one of claims 1 to 4 wherein the support is alumina or magnesium chloride.
- 6 A catalyst as claimed in any one of claims 1 to 5 wherein the lanthanide metal is Gadolinium or Erbium.
- 7 A catalyst as claimed in any one of claims 1 to 6 wherein the pi-arene complex is a 2:1 (arene:metal) complex.
- 8 A method of polymerising at least one olefin monomer which comprises bringing the olefin monomer(s) into contact with a catalytic amount of an olefin polymerisation catalyst as claime din any one of claims 1 to 7.
- 9 A method as claimed in claim 8 wherein the at least one olefin monomer is or includes propylene.

## INTERNATIONAL SEARCH REPORT

PCT/GB 92/00618

<b>I. CLASSIFICATION OF SUBJECT MATTER</b> (If several classification symbols apply, indicate all) <sup>6</sup>		
According to International Patent Classification (IPC) or to both National Classification and IPC		
Int.Cl. 5 C08F4/52; C08F4/02; C08F10/00		
<b>II. FIELDS SEARCHED</b>		
Minimum Documentation Searched <sup>7</sup>		
Classification System	Classification Symbols	
Int.Cl. 5	C08F	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched <sup>8</sup>		
<b>III. DOCUMENTS CONSIDERED TO BE RELEVANT<sup>9</sup></b>		
Category <sup>10</sup>	Citation of Document, <sup>11</sup> with indication, where appropriate, of the relevant passages <sup>12</sup>	Relevant to Claim No. <sup>13</sup>
Y	EP,A,0 295 829 (THE BRITISH PETROLEUM COMPANY P.L.C.) 21 December 1988 cited in the application see the whole document ---	1-9
Y	DE,A,2 653 379 (IMPERIAL CHEMICAL INDUSTRIES LTD.) 2 June 1977 see page 19 - page 27; claims 1,4-8 ---	1-9
A	US,A,4 665 046 (CAMPBELL,JR.) 12 May 1987 see claims ---	1-4
A	EP,A,0 371 664 (IMPERIAL CHEMICAL INDUSTRIES PLC) 6 June 1990 cited in the application see page 2, line 1 - page 8, line 18 --- -/--	1,5
<sup>10</sup> Special categories of cited documents : <sup>11</sup> "A" document defining the general state of the art which is not considered to be of particular relevance <sup>12</sup> "E" earlier document but published on or after the international filing date <sup>13</sup> "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) <sup>14</sup> "O" document referring to an oral disclosure, use, exhibition or other means <sup>15</sup> "P" document published prior to the international filing date but later than the priority date claimed <sup>16</sup> "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention <sup>17</sup> "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step <sup>18</sup> "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art <sup>19</sup> "G" document member of the same patent family		
<b>IV. CERTIFICATION</b>		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
17 AUGUST 1992	21. 08. 92	
International Searching Authority	Signature of Authorized Officer	
EUROPEAN PATENT OFFICE	KAUMANN, E. K.-H. <i>E. Kaumann</i>	

III. DOCUMENTS CONSIDERED TO BE RELEVANT (CONTINUED FROM THE SECOND SHEET)		
Category *	Citation of Document, with indication, where appropriate, of the relevant passages	Relevant to Claim No.
A	US,A,4 575 538 (HSIEH ET AL.) 11 March 1986 see the whole document ----	1,5

**ANNEX TO THE INTERNATIONAL SEARCH REPORT  
ON INTERNATIONAL PATENT APPLICATION NO. GB 9200618  
SA 58145**

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the European Patent Office EDP file on  
The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information. 17/08/92

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
EP-A-0295829	21-12-88	JP-A- 1025787	27-01-89
		US-A- 4894446	16-01-90
		US-A- 4973498	27-11-90
DE-A-2653379	02-06-77	GB-A- 1551016	22-08-79
		AU-B- 504656	25-10-79
		AU-A- 1987276	01-06-78
		BE-A- 848768	25-05-77
		FR-A, B 2338077	12-08-77
		JP-A- 52065800	31-05-77
		NL-A- 7613083	27-05-77
		US-A- 4121030	17-10-78
		US-A- 4299936	10-11-81
US-A-4665046	12-05-87	None	
EP-A-0371664	06-06-90	AU-B- 619061	16-01-92
		AU-A- 4562789	31-05-90
		JP-A- 3072952	28-03-91
		US-A- 5049534	17-09-91
		US-A- 5102964	07-04-92
US-A-4575538	11-03-86	None	